International Journal of Multidisciplinary and Scientific Emerging ResearcH (IJMSERH)

| ISSN: 2349-6037 | www.ijmserh.com ||Impact Factor: 9.274||Quarterly, Peer Reviewed & Refereed Journal|

|| Volume 12, Issue 3, July 2024 ||

Design of High Speed and High Head End Suction Pump

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ABSTRACT: Now a day due to vast change in industrial trend, pumping applications are switching over to high head requirements. At the same time industry demands for pump with simple construction, easy for maintenance with lowest possible price. For such applications multistage pump is the only conventional available option which has its own limitations like difficulties in maintenance, lesser efficiencies, more number of parts etc. However end suction pumps are easier for maintenance on account of its construction, are having comparatively higher efficiencies because of lower flow disturbances and are having less number of parts. If an end suction pump is forced to operate at higher speed, (2900 rpm and above) then the conventional end suction pumps can generate higher heads. The high speed end suction pumps will prove as a good replacement of medium pressure multistage pump.

KEYWORDS: End suction pump, high head, design of pump, volute casing, pump performance.

I. INTRODUCTION

Pump is a mechanical device used to transfer liquid from one location to another location. When impeller rotates in the casing it accelerates the fluid through its vanes and kinetic energy gets transferred from impeller to the fluid. In the pump casing the kinetic energy of fluid converted in to pressure energy.

Though the working principal of centrifugal pump is very simple, it has a wide application range of applications from small monoblock pumps with very less discharge to large vertical turbine or concrete volute pumps with thousands litres of discharge per second. Pumps are used for variety of pumping applications like water, acids, alkalis, brines, organic compounds etc.

When there is requirement of pump with high head, normally multistage pumps are offered. Function of a multi stage pump is similar to two or more number of pumps arranged in series. Fig 1 (a) shows sectional views of multistage pump. In multistage pumps numbers of impellers are arranged on single shaft. Each stage contains impeller, stage casing and diffuser. Each stage develops certain amount of head and numbers of stages are decided by dividing total head required with head developed per stage. For multistage pumps the total assembly is complicated and more number of parts with high machining accuracy is required as variation in dimension gets multiplied by number of stages. Also skilled labour required for pump assembly.

While searching out solution on these issues, it was found that only single stage end suction pump can overcome these problems but not capable of developing high heads. One more interesting thing triggered out that the high head requirement can be met by increasing driver speed as head developed by pump is proportional to the square of speed. If we increase the speed of pumps from 1500 to 3000 rpm the head obtained is approximately will be 4 times of the presently available head. The concept of doubling the speed considered and decided to implement it practically. All the components are newly designed to suit 3000 rpm as head becomes 4 times higher and torque and power becomes 8 times higher.

Fig 1(b) shows sectional view of end suction pump if we see fig1(a) and 1(b) we can say that end suction pump is very simple in construction as compared with multistage pump and the main challenge is to design and develop end suction pump to get desired output with satisfactory performance of pump.

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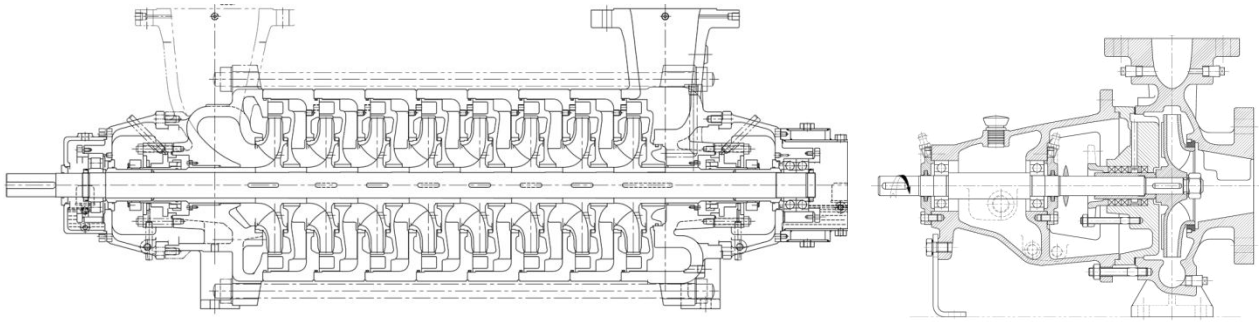


(a) (b)

Fig 1 Cross sectional drawing of (a) multistage pump (b) end suction pump

II. MATERIALS AND METHODS

The concept of doubling speed looks simple but a lot of technical aspects are required to be considered while doubling the speed. Since speed is doubled the tip or peripheral speed of impeller increased to 63.1m/s. For satisfactory working impeller, stainless is selected as impeller material. In multistage pumps initial stages are under low working pressures as pressure gets added step by step. However since this is single stage pump maximum allowable working pressure is considered as design criteria and accordingly SG Iron or stainless is decided as minimum material for pump casing. Based on earlier studies of failure analysis, stainless shaft grade SS316 is selected for further calculations as this material has good mechanical strength with high corrosion resistance.

Pump casing and impeller are cast components their manufacturing mythologies are as per standard procedure followed in pump industry i.e. deign, preparation of 3D drawing, pattern and core box manufacturing, preparation of moulds, metal pouring and machining of casting etc.

III. DEVELOPMENT OF HIGH SPEED PUMP

For development of high speed pump decided to select end suction pump whose mechanical design is suitable upto 1500 rpm. It was decided to redesign the pump in such a way that the pump can run at 3000rpm. This is very important aspect as due doubling the speed pump flow gets doubled, head developed by pump becomes 4 times higher and power requirement becomes 8 times higher.

Following steps followed.

1. Expected flow range, head value etc. decided as Flow between 200 to 350m^3/hr and head 205m or above. These inputs are based on current market scenario where multistage pumps are used for 200m and above head requirements.
2. New pump's specific speed calculated using formula, $Ns = \frac{N \times \sqrt{Q}}{H^{3/4}}$. Existing 4" end suction model finalised for redesign as specific speed of this 4" pump is close to new pump's specific speed. Expected performance calculated using affinity lawand curve plotted. Following figure shows the expected performance of pump.

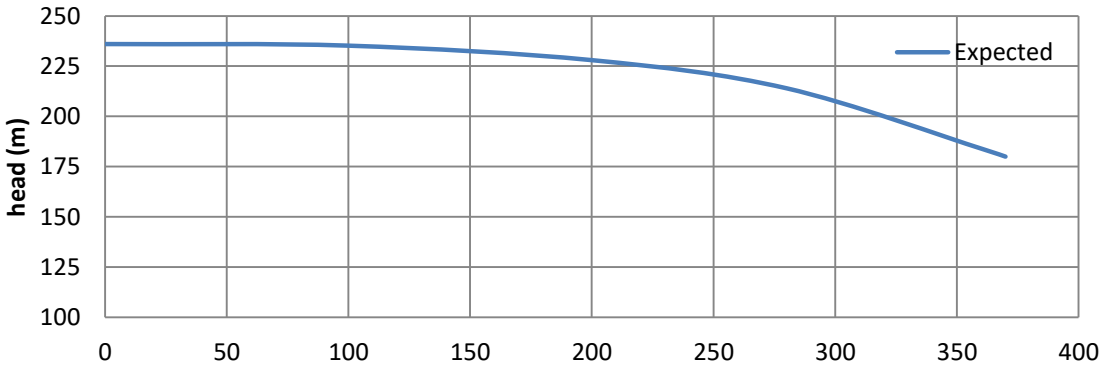


Fig 2 Expected pump performance

1. This is end suction pump and axial thrust exists due to unsymmetrical shape of impeller. Axial thrust calculated using formula mentioned in HI 1.3 standard and its value is FA = 9850.84232 N
2. Radial thrust(F_R) acts on impeller. As liquid flows through volute area, velocity head gets converted to pressure head and exerts pressure on impeller peripheral area and volute wall.

$FR = K_R \times H \times \rho \times g \times D2 \times B$

Where, K_R= Thrust factor,

H = Head developed by pump = 205m

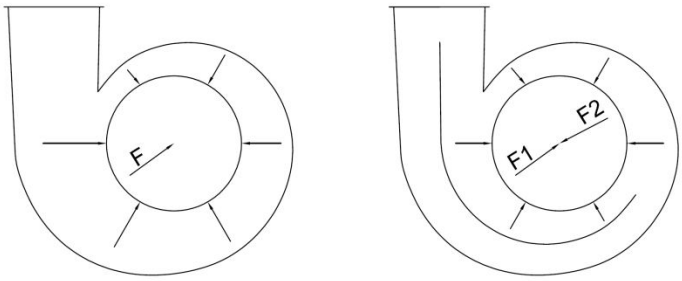
ρ = density of liquid = 1060Kg/m3

g = Gravitational constant (9.81 m/s2)

D2 = Diameter of impeller = 0.409m

B = Width of impeller= 0.015m

Fig 3(a) is single volute design it is unsymmetrical but easy for manufacturing, there are chances of higher radial thrust on impeller. Fig 3(b) is double volute design it is more symmetrical than single volute due to this major part of thrust acting on impeller get balanced but more foundry skill involved in pattern making and manufacturing.

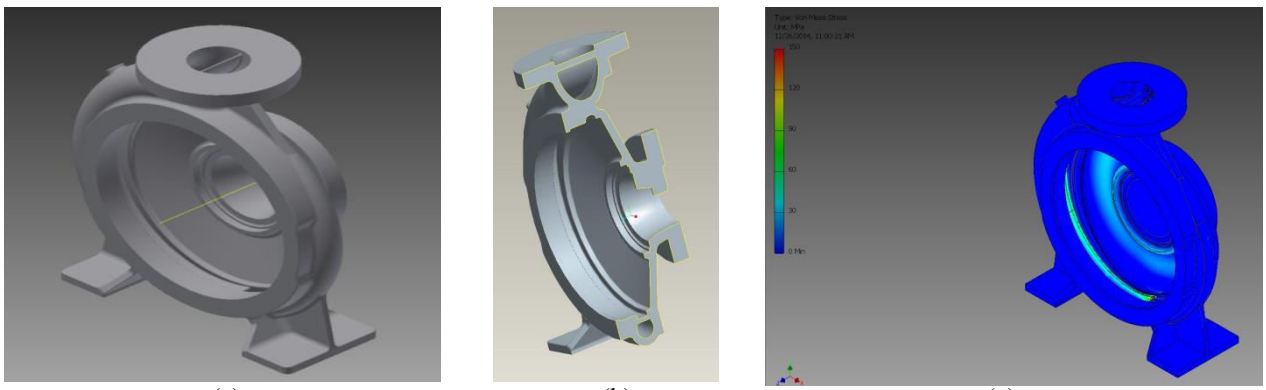


(a) (b)

Fig 3Volute casing types (a)Single Volute (b) Double Volute

Radial thrust factor calculated for single volute casing. Thrust value is considerably high i.e. 1830.92N. This resulted into higher bearing sizes and shaft diameter. To optimize the design, calculations carried out for double volute casings.Due to symmetrical design of double volute, thrust factor $K_R$is small. Thrust coming on impeller is 588.51N. This is considerably low as compared with single volute. So double volute design finalised.

1. Using pressure vessel analogy pump casing is designed. 3D model of the casing is prepared.Fig 4(a) and (b) shows 3D model of casing and cut sectional view of casing respectively. After preparation of 3D model, stress analysis of casing carried out by applying pressure in inner part of casing. Stress analysis carried out in Autodesk Inventor software. Fig 4(c) shows stress analysis results.



(a) (b) (c)

Fig 4 Volute casing 3D model (a) Standard View (b) Cut Section (c) Stress analysis results

2. Shaft Design – Refer Fig 5(a). Free body diagram of shaft is drawn. Shear force and bending moment values are calculated. Based on these shaft design is done. Maximum deflection of shaft is calculated using formula$y_{max}=\frac{F\,(a^3-a^2 l)}{3\,EI}$. Deflection values are cross checked using Autodesk Inventor (Refer Fig 5(b)).

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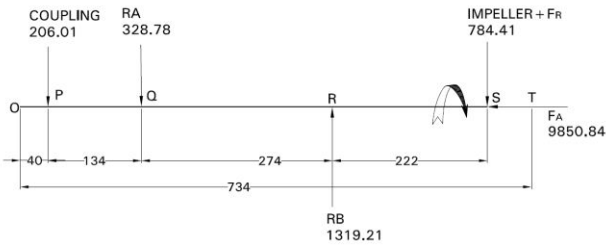
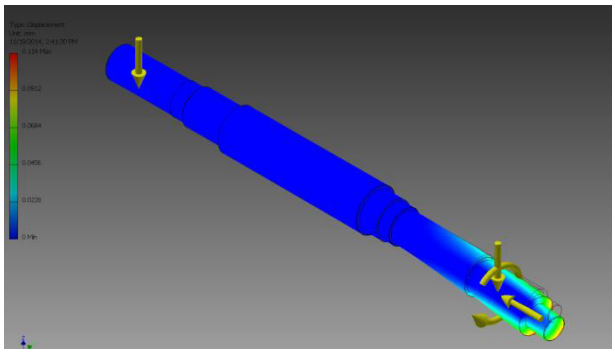


(a)



(b)

Fig 5 Shaft design (a) free body diagram (b) Deflection by Autodesk inventor

3. Critical speed of Pump – For this newly designed pump critical speed calculated using formula,

$N_{cr} = \frac{1}{2\pi}\sqrt{\frac{K}{m}}$

$N_{cr} = \frac{1}{2\pi}\sqrt{\frac{mg/ymax}{m}} = \frac{1}{2\pi}\sqrt{\frac{g}{ymax}}$

N_{cr}= 157Hz = 9420 rpm

The newly designed high speed pump speed(N) is 3000RPM. As per guidelines from various pump handbooks and vibration related literatures the operating speed should not close to critical speed, it should be lesser than 0.8Ncr or more than 1.3 times critical speed (N_{cr}). This helps to avid abnormal vibrations due to resonance. For this newly designed pump, speed (N) is far away from resonance speed band.

4. Using all these calculation results, detailed design of pump is carried out. Major component's designs validated by carrying stress analysis. The stress analysis and design calculation results found close to each other.

IV. MANUFACTURING AND EXPERIMENTAL TESTING

1. This end suction pump manufactured using various process followed in pump manufacturing industry.
2. The pump tested in pump testing laboratory. Fig 6(a) shows pump testing setup at testing laboratory. Parameters like head, power, bearing temperatures vibrations etc. measured for various flows. Finally performance curve of newly designed curve established. Fig 6(b) is performance curve of the newly designed pump.

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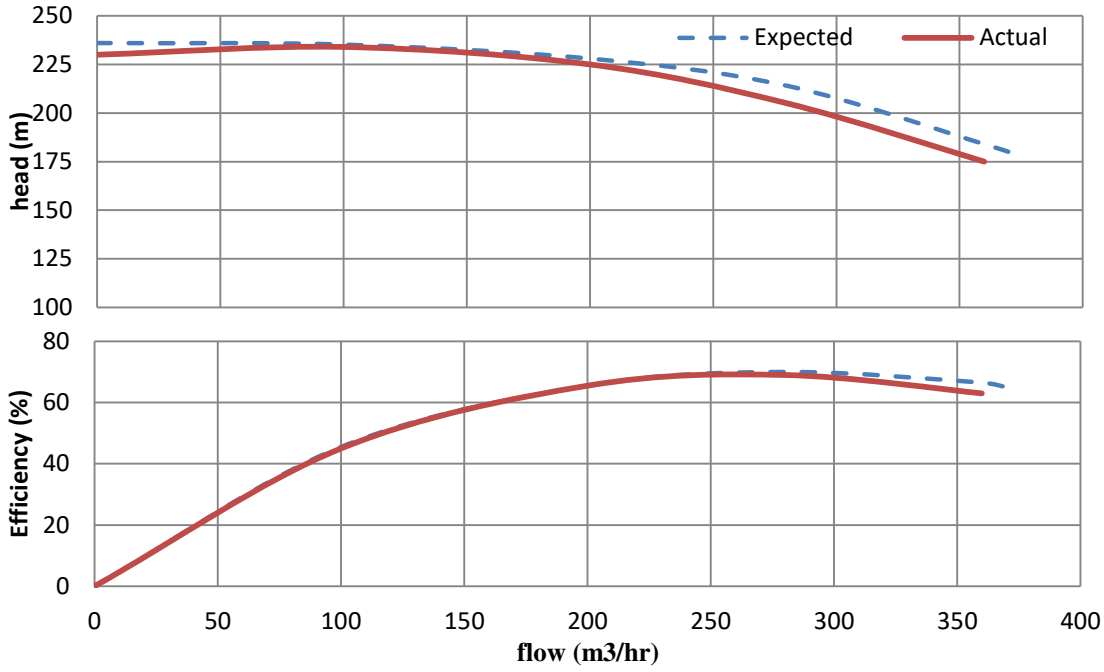
(a)



(b)

Fig 6(a) Pump performance test setup (b) Performance curve

V. CONCLUSION

The newly designed high speed high head end suction pump achieved the required duties mentioned. The overall hydraulic performance of pump is very close to expected values. The values of bearing temperatures, noise and vibration levels observed during performance are well within acceptable limits. This type of design made the pump compact, easy to assemble, less number of parts and economical as compared to conventional multistage pump. Double volute construction reduces the total radial load on the rotating unit. It reduces the shaft and bearing size as compare to conventional pump.For the future growth expected in process sectorthis development of high head high speed process

pump has given the competent solution.In nutshell the high speed end suction pumps will prove as a good replacement of medium pressure multistage pump.

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